Supporting Information for

Towards quantitative and scalable transformation of furfural to cyclopentanone with supported gold catalysts

Gao-Shuo Zhang, Ming-Ming Zhu, Qi Zhang, Yong-Mei Liu, He-Yong He, and Yong Cao*

Department of Chemistry, Shanghai Key Laboratory of Molecular Catalysis and Innovative Materials, Fudan University, Shanghai 200433, P. R. China

E-mail: yongcao@fudan.edu.cn

| Entry | Additive | Conv. [%] | Mass balance [%] | Sel. [%] | | | | | |
|-------|----------------------------------|-----------|-------------------|----------|-----|----|-----|------|--|
| | | | Mass balance [70] | СРО | CPL | MF | FAL | CEON | |
| 1 | Na ₂ CO ₃ | >99 | 27±5 | 0 | 0 | 3 | 24 | 0 | |
| 2 | Na ₂ HPO ₄ | >99 | 48±3 | 0 | 0 | 7 | 41 | 0 | |
| 3 | none | >99 | 99±1 | >99 | 0 | 0 | 0 | 0 | |
| 4 | NaH ₂ PO ₄ | >99 | 64±3 | 47 | 1 | 0 | 11 | 5 | |
| 5 | H_3PO_4 | >99 | 31±5 | 19 | 2 | 0 | 4 | 6 | |

Table S1. Effect of additives on the transformation of furfural (FFA) over 0.73 wt% Au/TiO2-A.[a]

[a] Reaction conditions: FFA (5.2 mmol), H₂O (10 mL), additive (0.1 mmol), H₂ (4 MPa), S/C (2000), 160 °C, 1.2 h.

Table S2. The hydrogenation of FFA over platinum-group-metal (PGM)-based catalysts.^[a]

| Entry | catalvet[b] | Conv. [%] | Mass balance [%] | Sel. [%] | | | | | |
|-------|-----------------------------------|-----------|---------------------|----------|-----|----|-----|------|--|
| | catalyst | | | СРО | CPL | MF | FAL | CEON | |
| 1 | Pt/TiO ₂ -A (0.73 wt%) | 87 | 87±3 | 71 | 5 | 11 | 0 | 0 | |
| 2 | Pd/TiO ₂ -A (0.73 wt%) | 23 | 95±2 | 87 | 1 | 6 | 0 | 1 | |
| 3 | Ir/TiO ₂ -A (0.73 wt%) | 56 | 93±2 | 34 | 0 | 0 | 0 | 59 | |
| 4 | Rh/TiO ₂ -A (0.73 wt%) | 41 | 94±2 | 93 | 0 | 0 | 0 | 1 | |

[a] Reaction conditions: FFA (5.2 mmol), H₂O (10 mL), H₂ (4 MPa), S/C (2000), 160 °C, 1.2 h.

Table S3. The hydrogenation of FFA over TiO2-A supported noble catalysts at 80 °C.^[a]

| Entry | catalvet | Conv [%] | Sel. [%] | | |
|-------|-----------------------------------|----------|----------|-------|--|
| | Catalyst | | FAL | other | |
| 1 | Au/TiO ₂ -A (0.73 wt%) | 31 | 99 | 0 | |
| 2 | Pt/TiO ₂ -A (0.73 wt%) | 82 | 99 | 0 | |
| 3 | Pd/TiO ₂ -A (0.73 wt%) | 63 | 99 | 0 | |

[a] Reaction conditions: FFA (5.2 mmol), H₂O (10 mL), H₂ (4 MPa), S/C (2000), 80 °C, 1.2 h.

Table S4. The effect of different-sized gold particles and various gold loadings on the transformation of FFA to CPO.^[a]

| Entry | Catalyst | Average | Conv. [%] | TOF ^[b] | Mass balance [%] | Sel. [%] | | | |
|--------|----------|-----------|--------------|--------------------|------------------------|----------|-----|-----|------|
| Linu y | | size [nm] | | $[h^{-1}]$ | | СРО | CPL | FAL | CEON |

| 1 | Au/TiO ₂ -A (0.73wt%) | 2.1 | >99 | 7520 | 99±1 | >99 | 0 | 0 | 0 |
|---|----------------------------------|--------------------|-----|------|------|-----|---|----|----|
| 2 | Au/TiO ₂ -A (0.71wt%) | 4.6 ^[c] | 35 | 680 | 99±1 | 36 | 0 | 25 | 38 |
| 3 | Au/TiO ₂ -A (0.75wt%) | 8.4 ^[d] | 16 | 270 | 99±1 | 25 | 0 | 28 | 46 |
| 4 | Au/TiO ₂ -A (0.24wt%) | 2.1 | >99 | 7560 | 99±1 | >99 | 0 | 0 | 0 |
| 5 | Au/TiO ₂ -A (0.10wt%) | 2.0 | >99 | 7470 | 99±1 | >99 | 0 | 0 | 0 |

[a] Reaction conditions: FFA (5.2 mmol), H₂O (10 mL), H₂ (4 MPa), S/C (2000), 160 °C, 1.2 h; [b] TOF values based on total the gold loading at FFA conversion of 15%; [c] Figure S9e; [d] Figure S9f.



Figure S1. Reaction profiles for the hydrogenation of FFA over a series of Au/TiO₂-A catalysts with different gold loading content or S/C levels. (a) 0.24 wt% Au/TiO₂- A (S/C~2000); (b) 0.73 wt% Au/TiO₂-A mixed with seven-fold bare TiO₂-A (S/C~2000); (c) 0.24 wt% Au/TiO₂-A (S/C~10000); (d) 0.73 wt% Au/TiO₂-A (S/C~10000). Reaction condition: FFA (5.2 mmol), H₂O (10 mL), H₂ (4 MPa), 160 °C.

Table S5. The effect of reaction temperature and hydrgen pressure on the transformation of FFA to CPO over 0.10 wt% Au/TiO₂-A.^[a]

| Entry | H ₂ [MPa] | /IPa] T [ºC] | Conv. [%] | Mass balance [%] | Sel. [%] | | | | |
|-------|----------------------|--------------|-----------|-------------------|----------|-----|-----|------|--|
| | | | | Mass balance [70] | СРО | CPL | FAL | CEON | |
| 1 | 4 | 120 | 42 | 99±1 | 18 | 0 | 71 | 10 | |
| 2 | 4 | 140 | 77 | 99±1 | 76 | 0 | 10 | 13 | |
| 3 | 4 | 160 | >99 | 99±1 | >99 | 0 | 0 | 0 | |
| 4 | 4 | 180 | >99 | 95±2 | 88 | 7 | 0 | 0 | |
| 5 | 3 | 160 | 92 | 99±1 | 86 | 0 | 0 | 13 | |
| 6 | 5 | 160 | >99 | 99±1 | 96 | 3 | 0 | 0 | |

[a] Reaction conditions: FFA (5.2 mmol), $\rm H_2O$ (10 mL), S/C (2000), 1.2 h.





Figure S2. NH₃-TPD profiles of various supports and gold catalysts.



Figure S3. FTIR spectra of pyridine adsorbed onto the various oxide supports.



Figure S4. Kinetic profiles of 50 mmol scale. Reaction condition: FFA (50 mmol), catalyst (0.10 wt% Au/TiO₂-A), H₂O (100 mL), H₂ (4 MPa), S/C (20000), 160 °C.



Figure S5. Dependence of the initial reaction rates on the catalyst concentration for the transformation of furfural. Reaction condition: FFA (50 mmol), H_2O (100 mL), H_2 (4 MPa), catalyst (0.10 wt% Au/TiO₂-A), 160 °C, conversion of FFA (15%).



Figure S6. Powder XRD patterns of various Au/TiO₂ catalysts.



Figure S7. XANES analysis of Au/TiO₂-A catalyst.











Figure S8. TEM analysis of various catalysts (a) $0.10 \text{ wt\% Au/TiO}_2$ -A; (b) $0.10 \text{ wt\% Au/TiO}_2$ -A-reused; (c) $0.24 \text{ wt\% Au/TiO}_2$ -A; (d) $0.73 \text{ wt\% Au/TiO}_2$ -A; (e) $0.71 \text{ wt\% Au/TiO}_2$ -A (4.6 nm); (f) $0.75 \text{ wt\% Au/TiO}_2$ -A (8.4 nm); (g) $0.63 \text{ wt\% Au/TiO}_2$ -R; (h) $0.62 \text{ wt\% Au/TiO}_2$ -P25; (i) $0.85 \text{ wt\% Au/Al}_2$ O₃; (j) $0.65 \text{ wt\% Au/SiO}_2$; (k) $0.68 \text{ wt\% Au/ZrO}_2$; (l) 0.64 wt% Au/HY; (m) 0.62 wt% Au/H-ZSM-5; (n) $0.61 \text{ wt\% Au/Nb}_2$ O₅.



Figure S9. XRD analysis of various forms of nanostructured CeO₂.





Figure S10. TEM analysis of various forms of nanostructured CeO₂. (a) CeO₂-nanorods; (b) CeO₂-90; (c) CeO₂-octahedra; (d) CeO₂-cube; (e) CeO₂-meso; (f) CeO₂-nps; (g) CeO₂-nanorods-used.